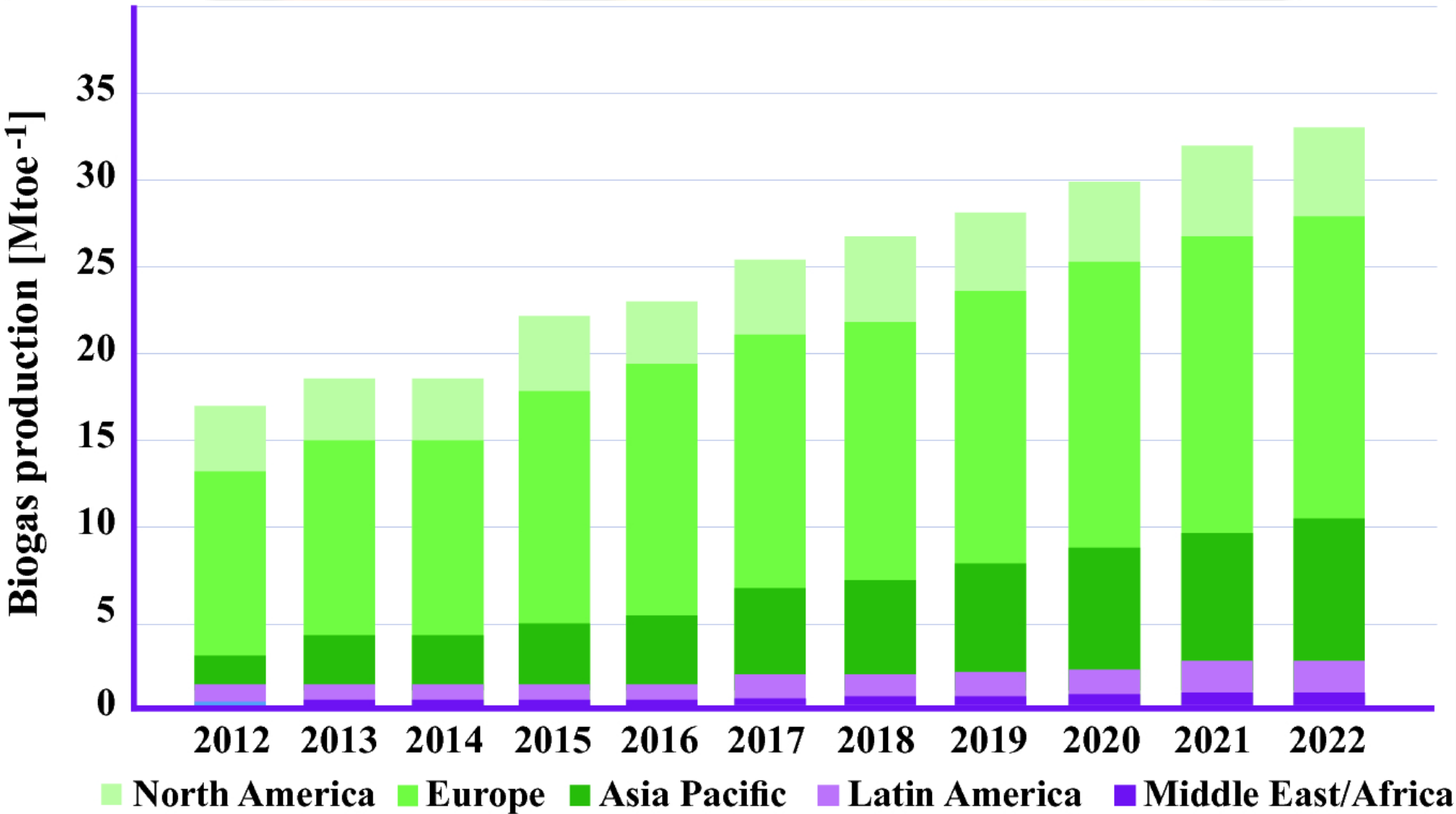


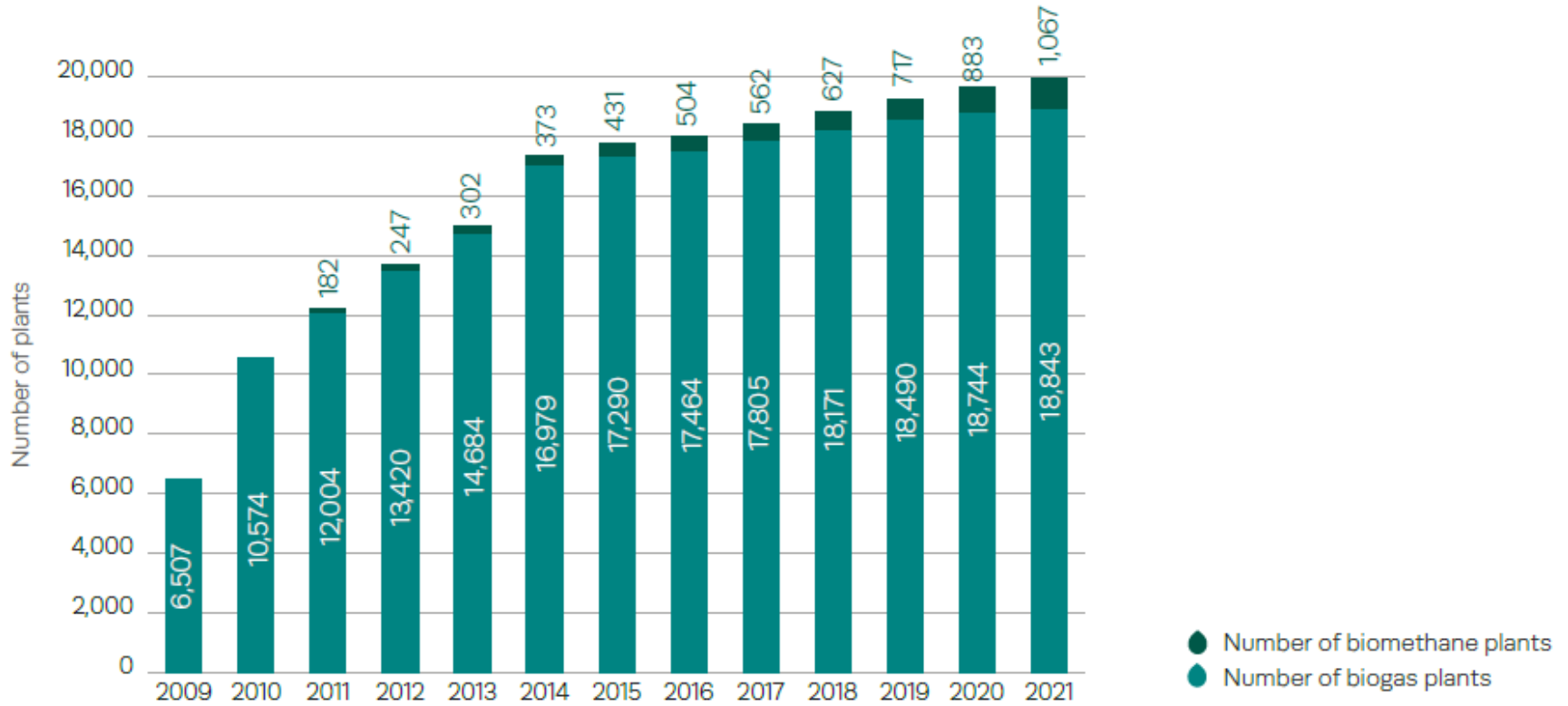
# Microalgae-based biogas upgrading: a sustainability driven technology

**Raúl Muñoz** ([raul.munoz.torre@uva.es](mailto:raul.munoz.torre@uva.es))

Institute of Sustainable Processes-Valladolid University

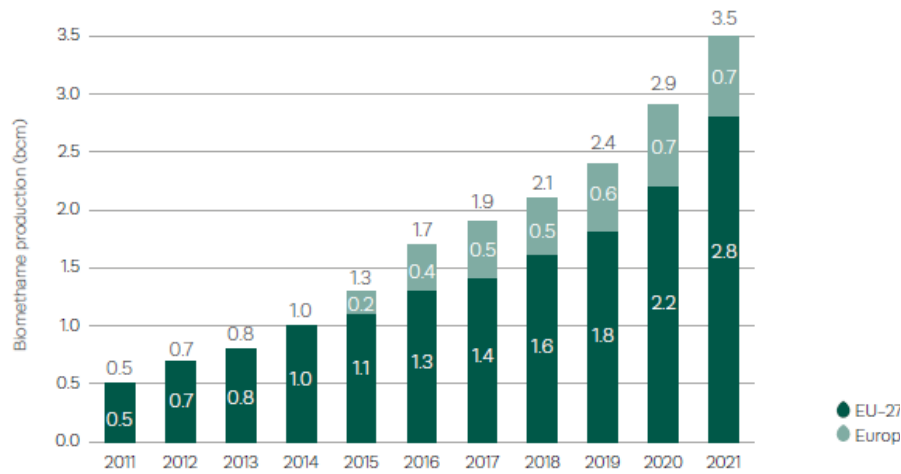




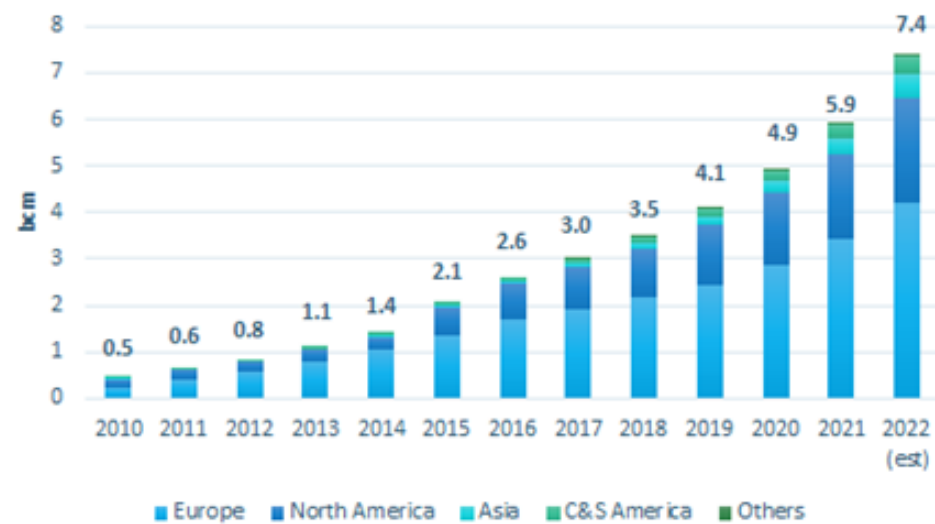


(EBA, 2021)

## Europe

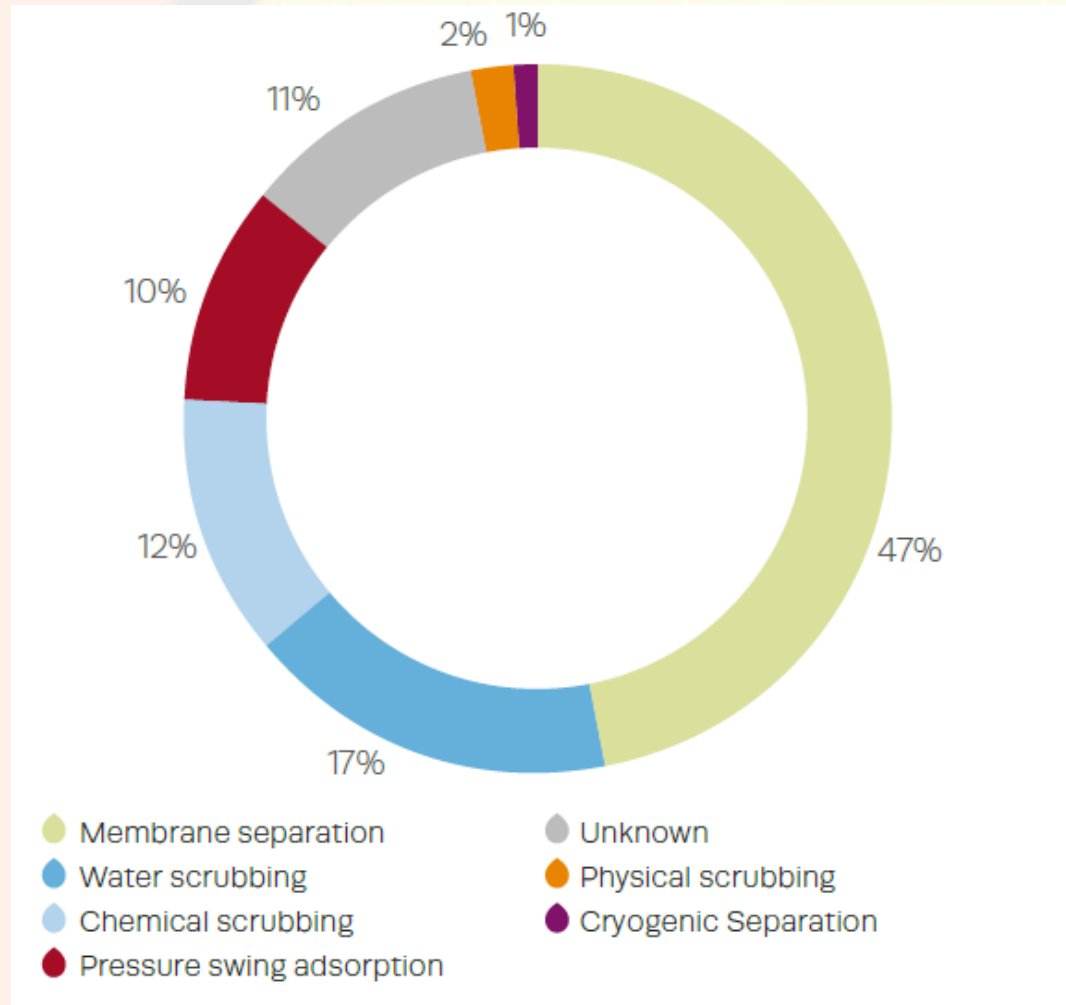


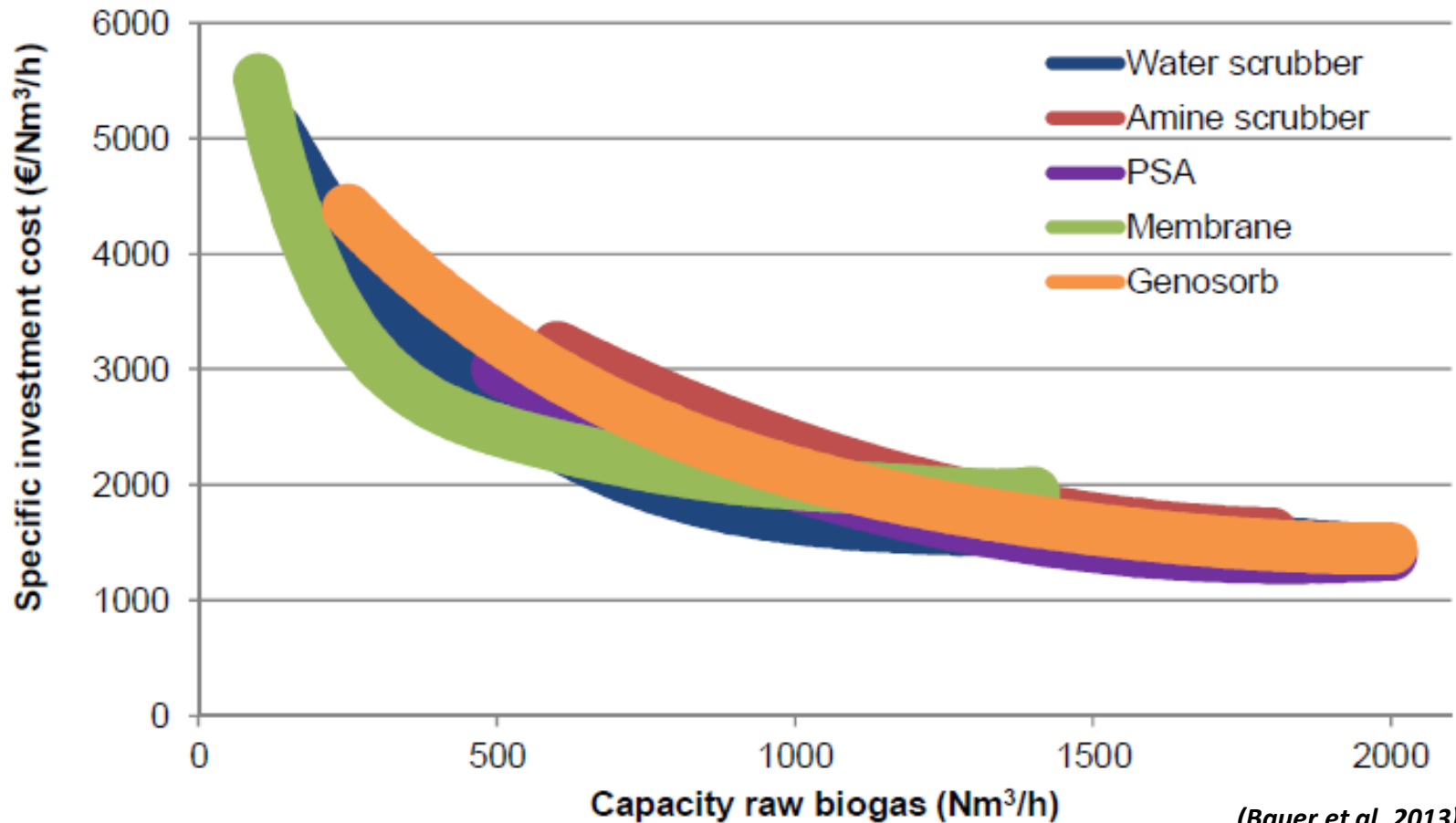
## World



(EBA, 2022)

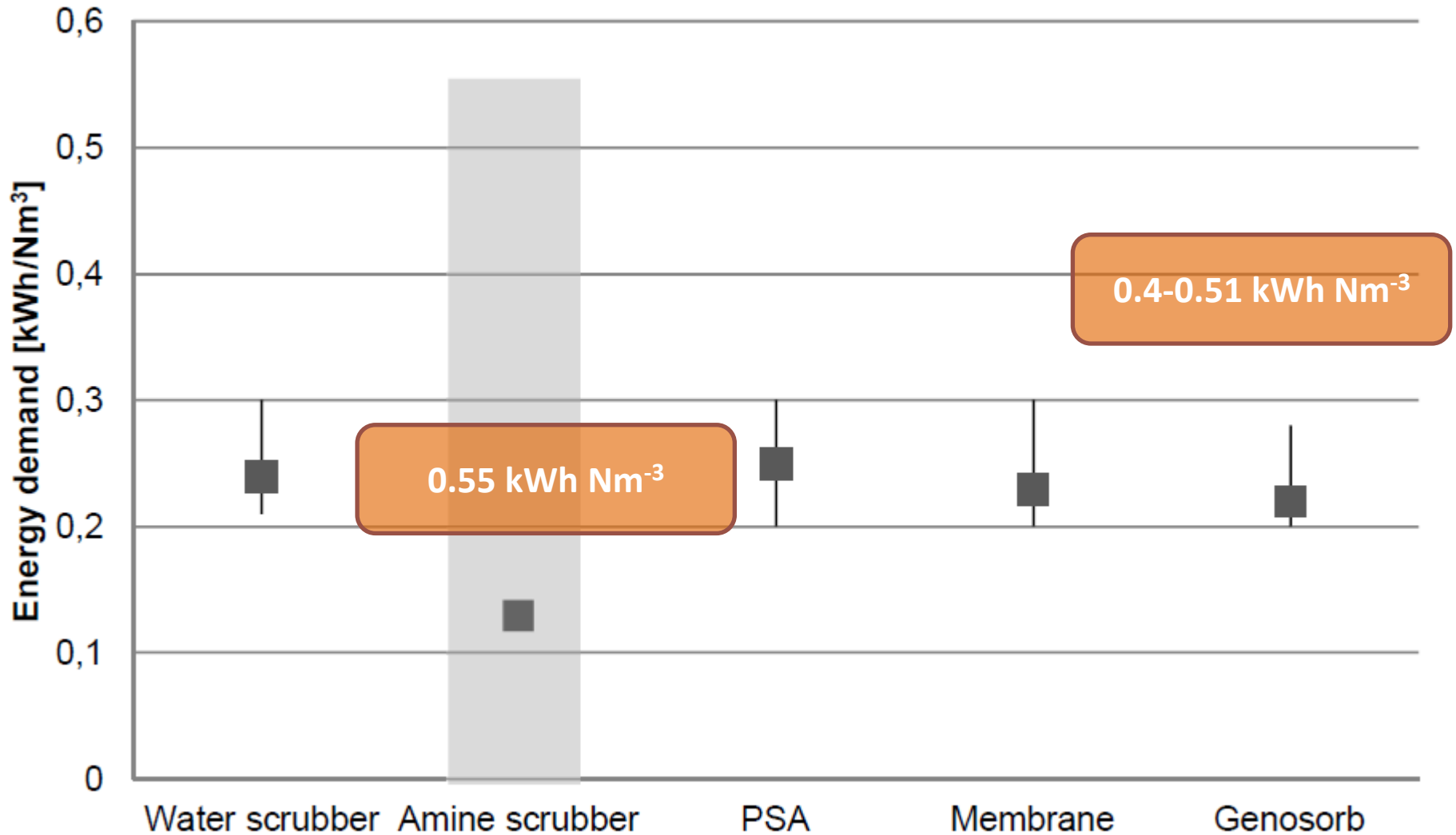
**Today....**





(Bauer et al. 2013)

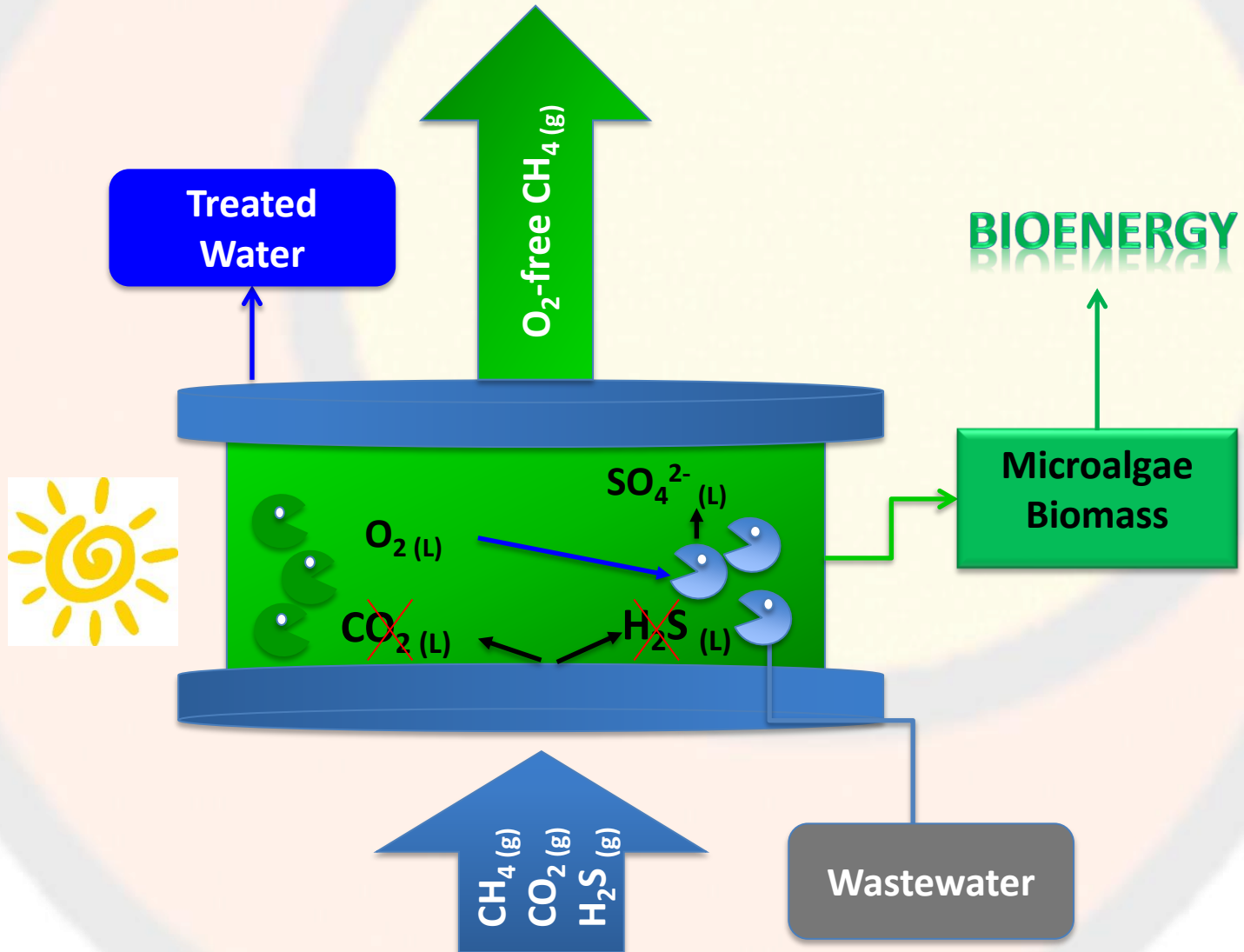
Energy demand: 3-12 % energy content of **Biogas**

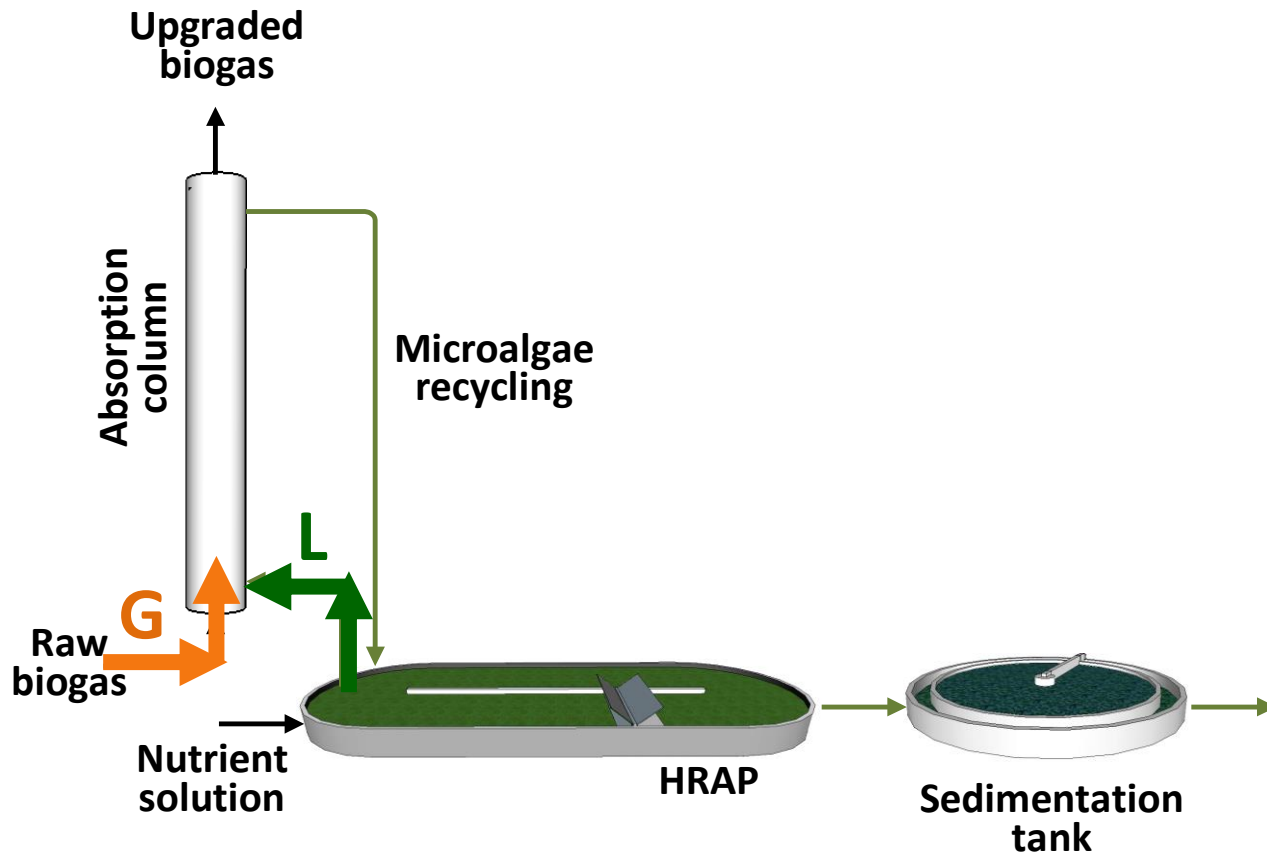


*Need to develop innovative  
low-cost & environmentally  
friendly technologies for a  
sustainable **Biogas**  
upgrading at small-medium  
scale*



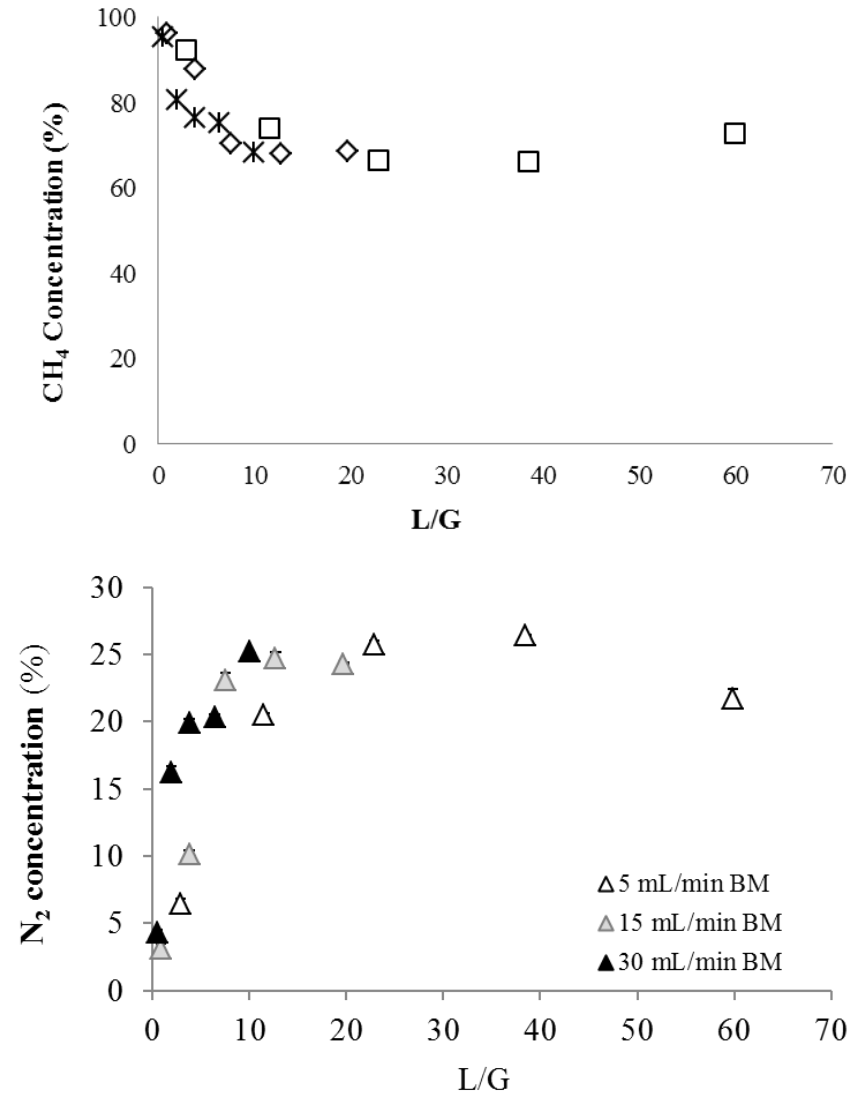
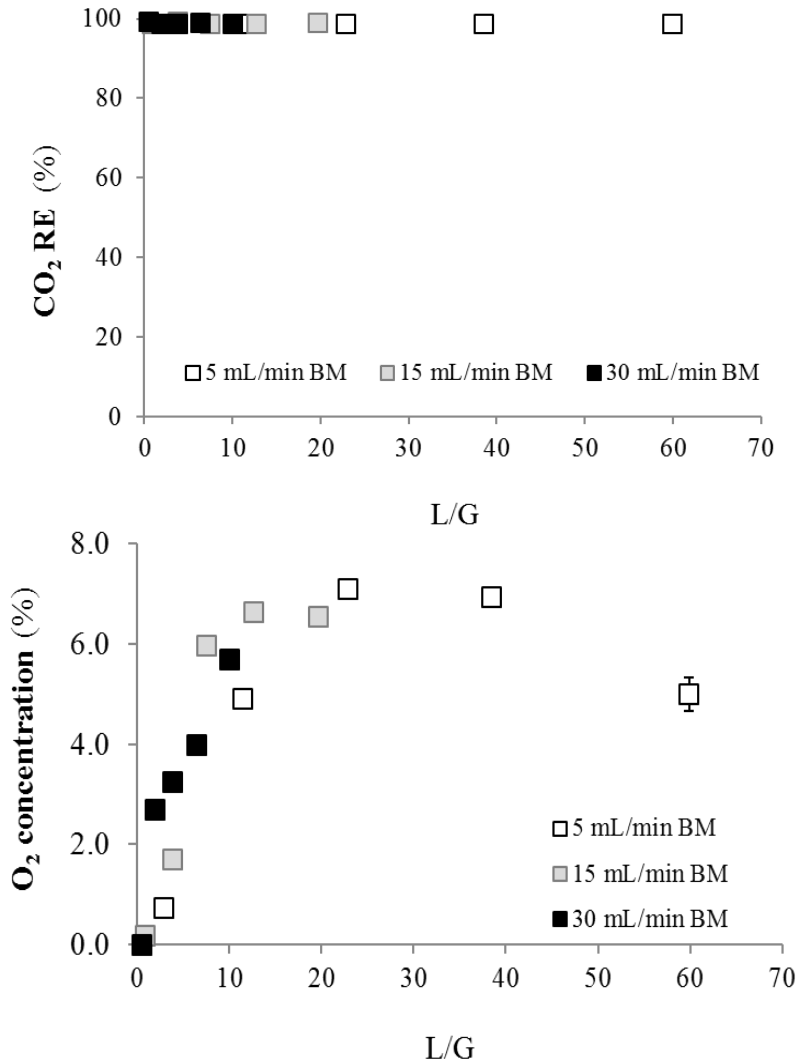




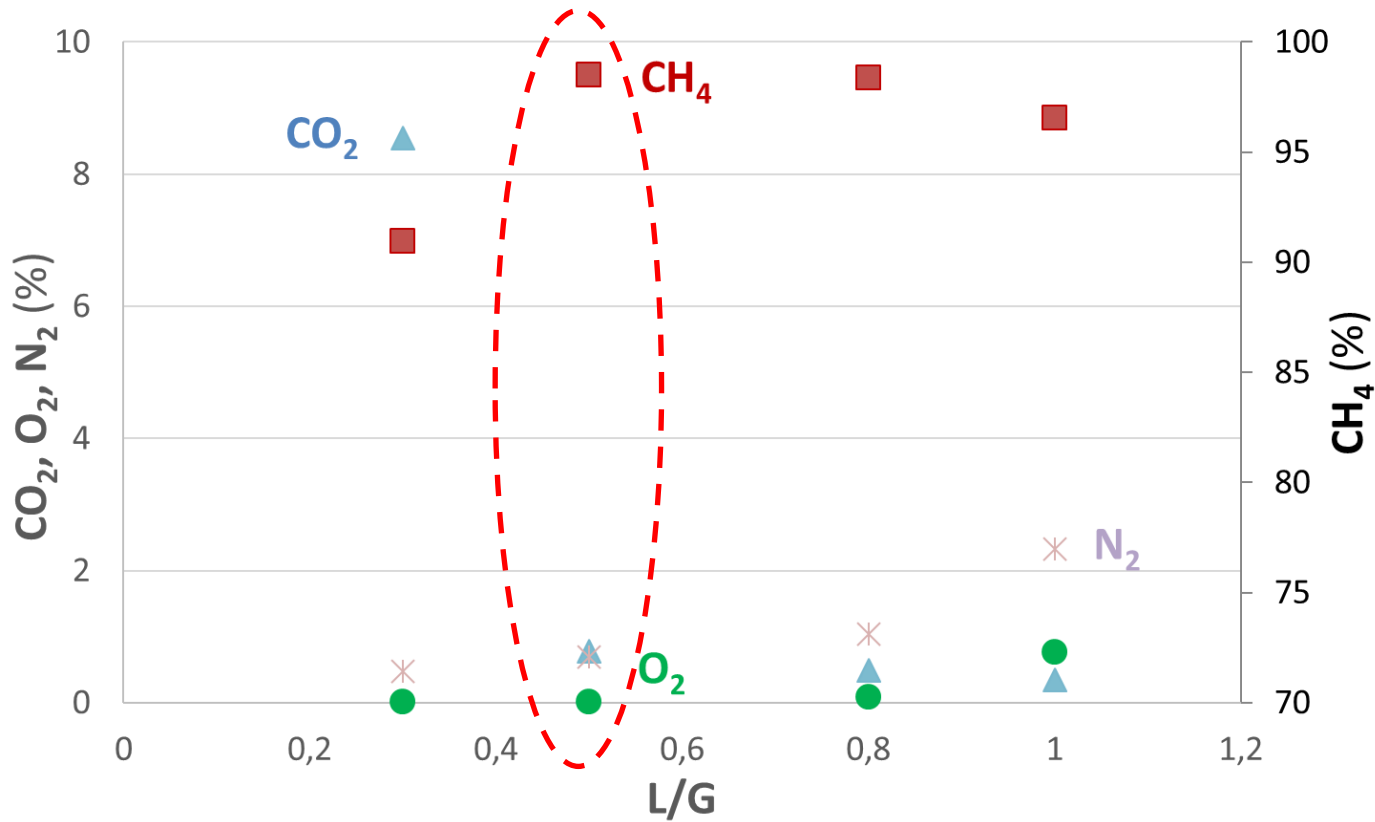


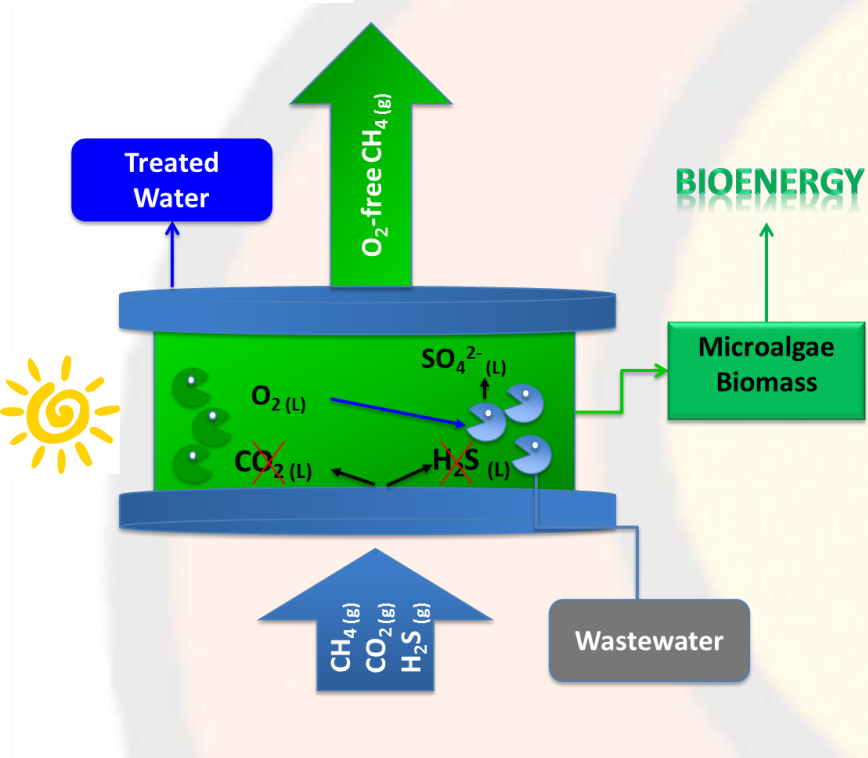
Key operational parameter: **Recycling Liquid/Biogas** ratio

## INFLUENCE OF L/G RATIO

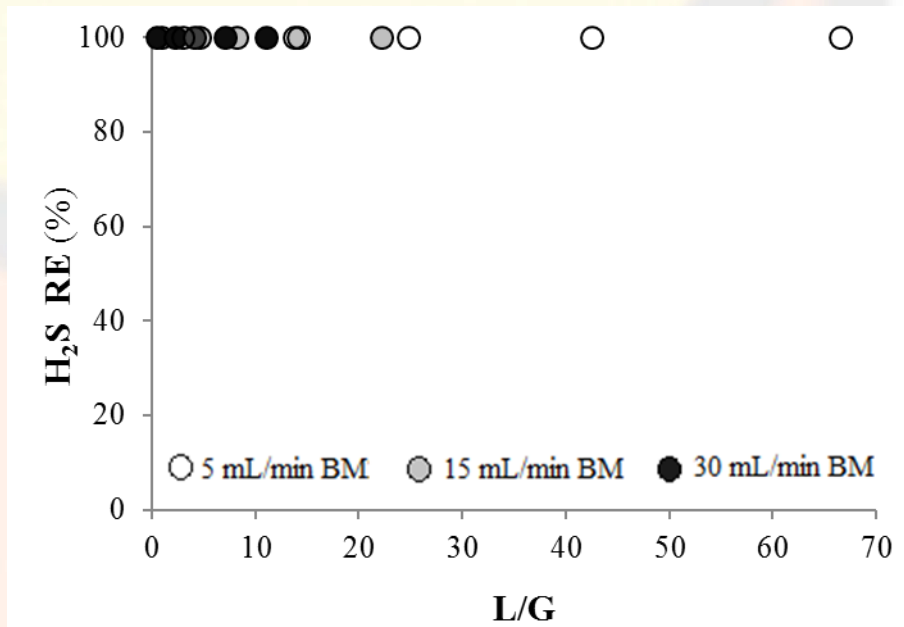
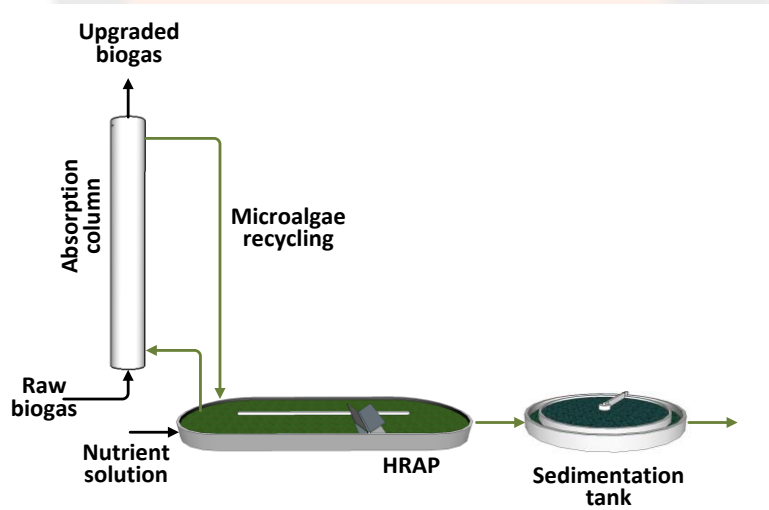


## INFLUENCE OF L/G RATIO

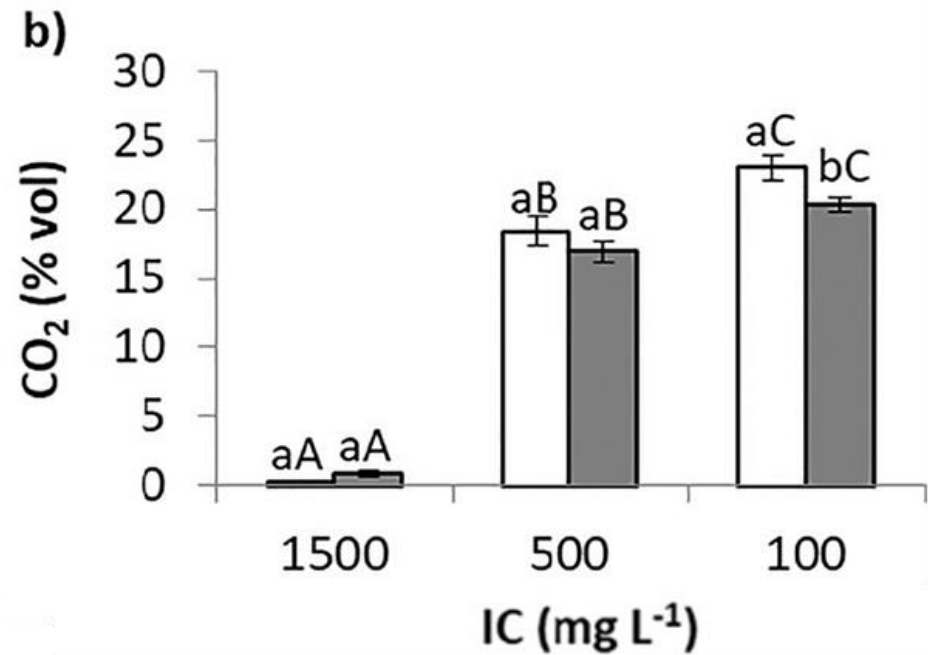
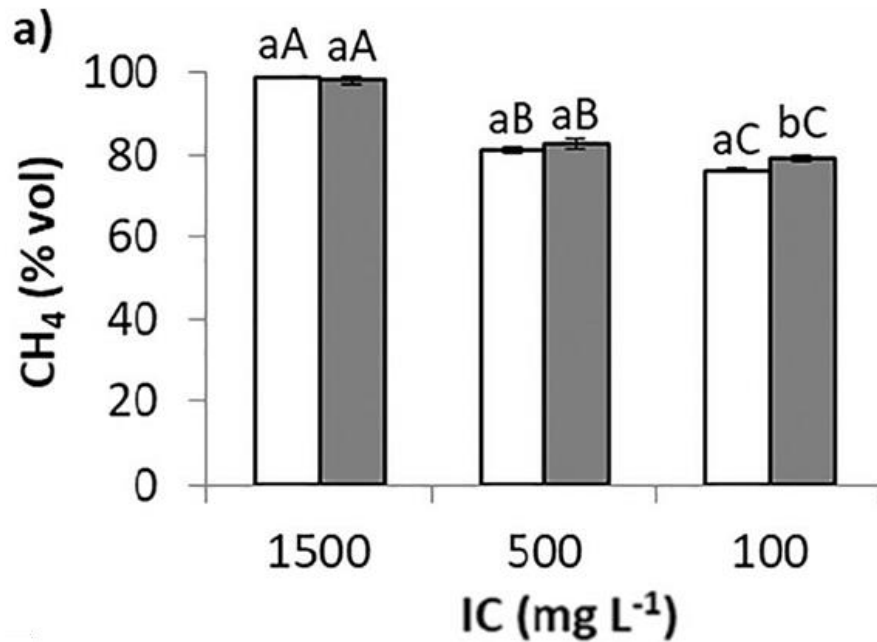


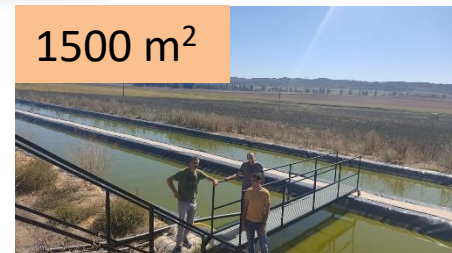


- The high pH value → High H<sub>2</sub>S mass transfer
- RE-H<sub>2</sub>S > 99 %



## INFLUENCE OF ALKALINITY AND TEMPERATURE







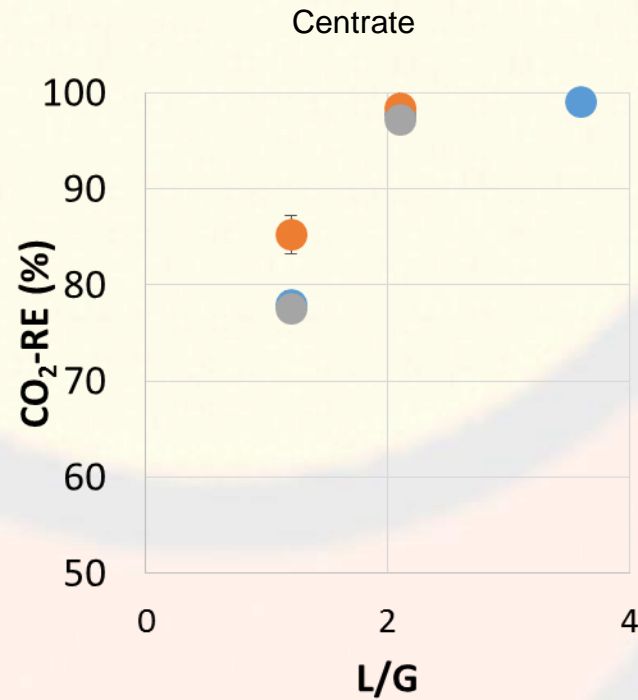
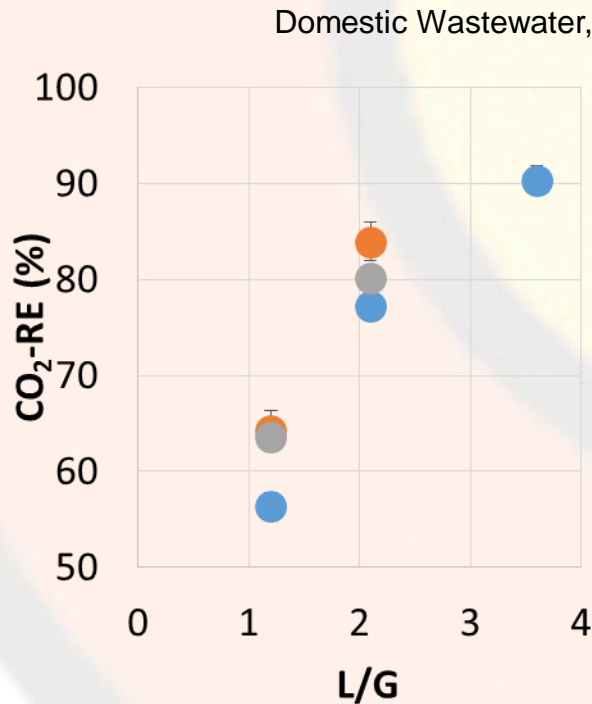
DEMO PILOT PLANT IN  
CHICLANA



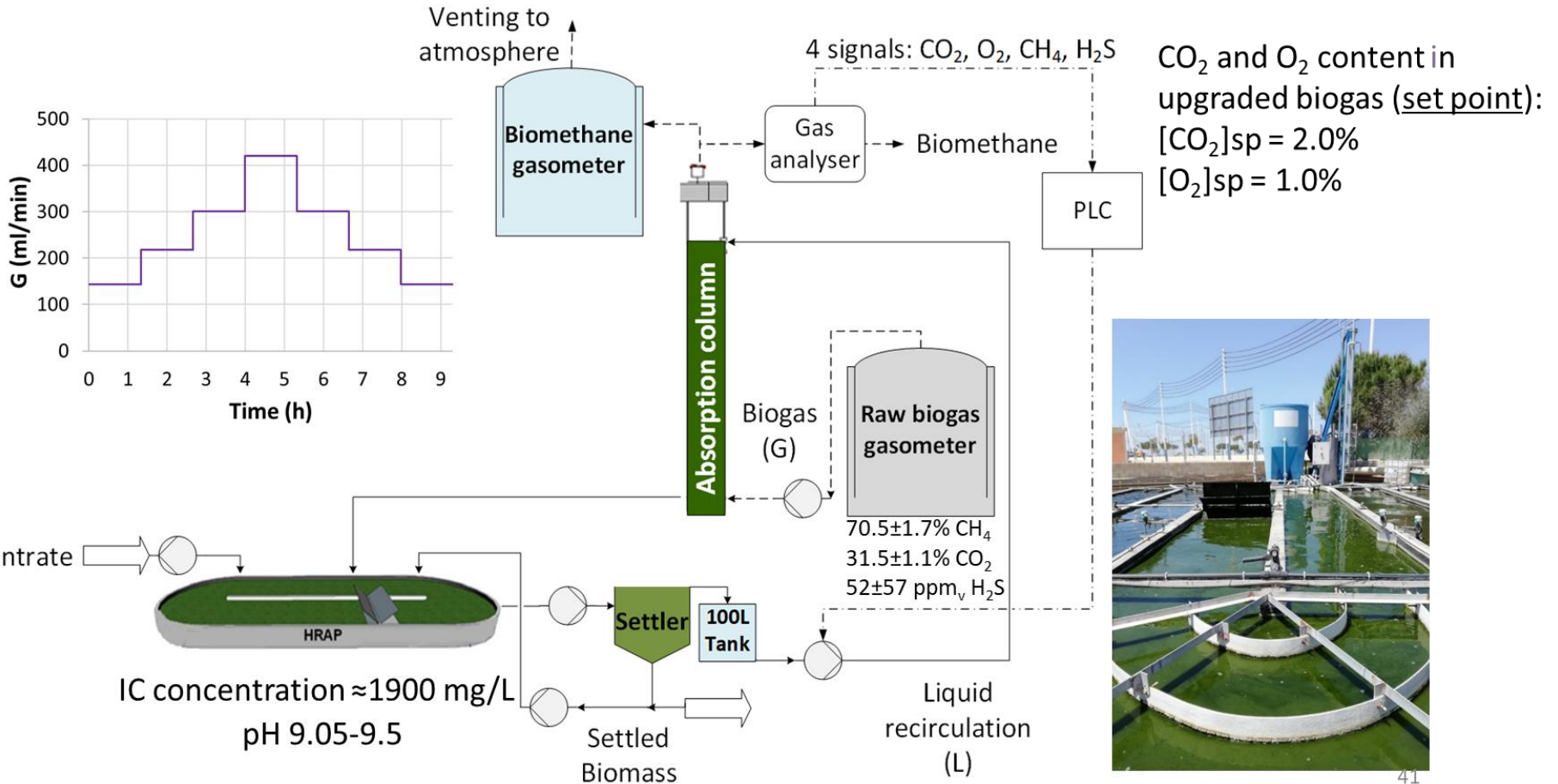


## DEMO PLANT at Chiclana de la Frontera

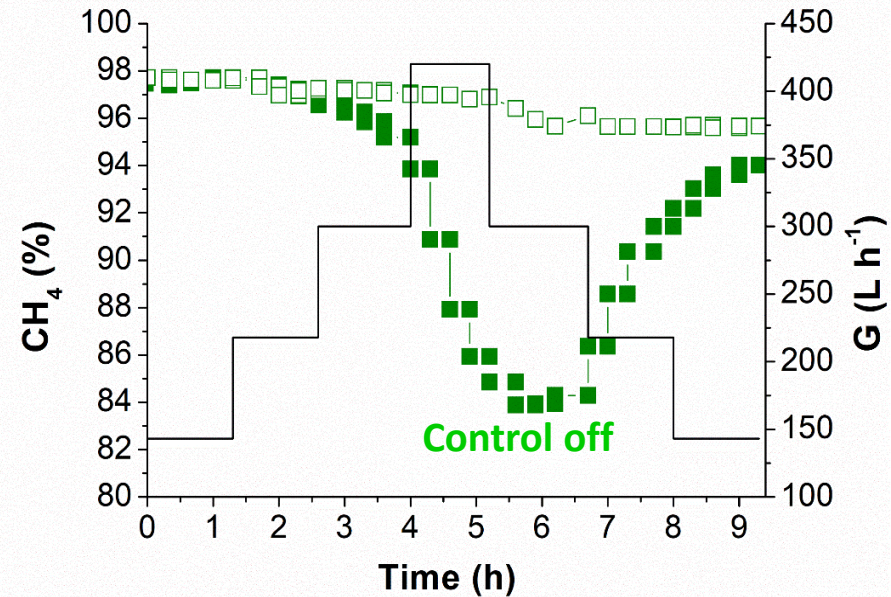
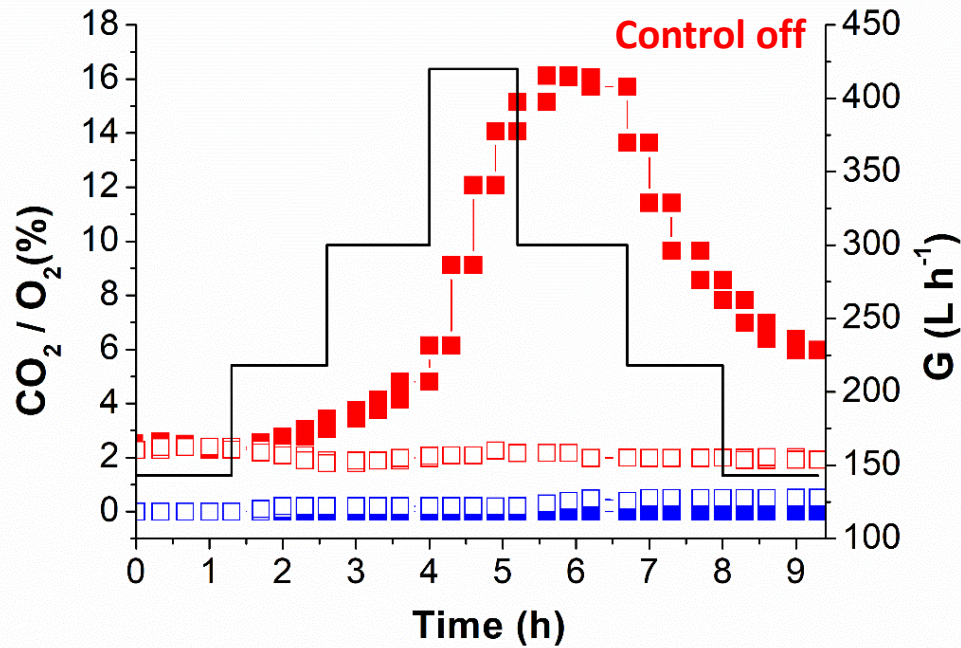
CO<sub>2</sub> removal efficiencies at biogas flowrate of 274±12 (●), 370 ±7(●) and 459 ±36 (●) L/h



## PROCESS CONTROL



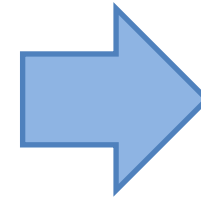
## ROBUSTNESS TOWARDS BIOGAS FLOW RATE VARIATIONS



# Photosynthetic Biogas Upgrading & Nutrient Recovery



N = 600-4000 mg/L  
P = 100-500 mg/L



[Microalgae]=7-50 g/L

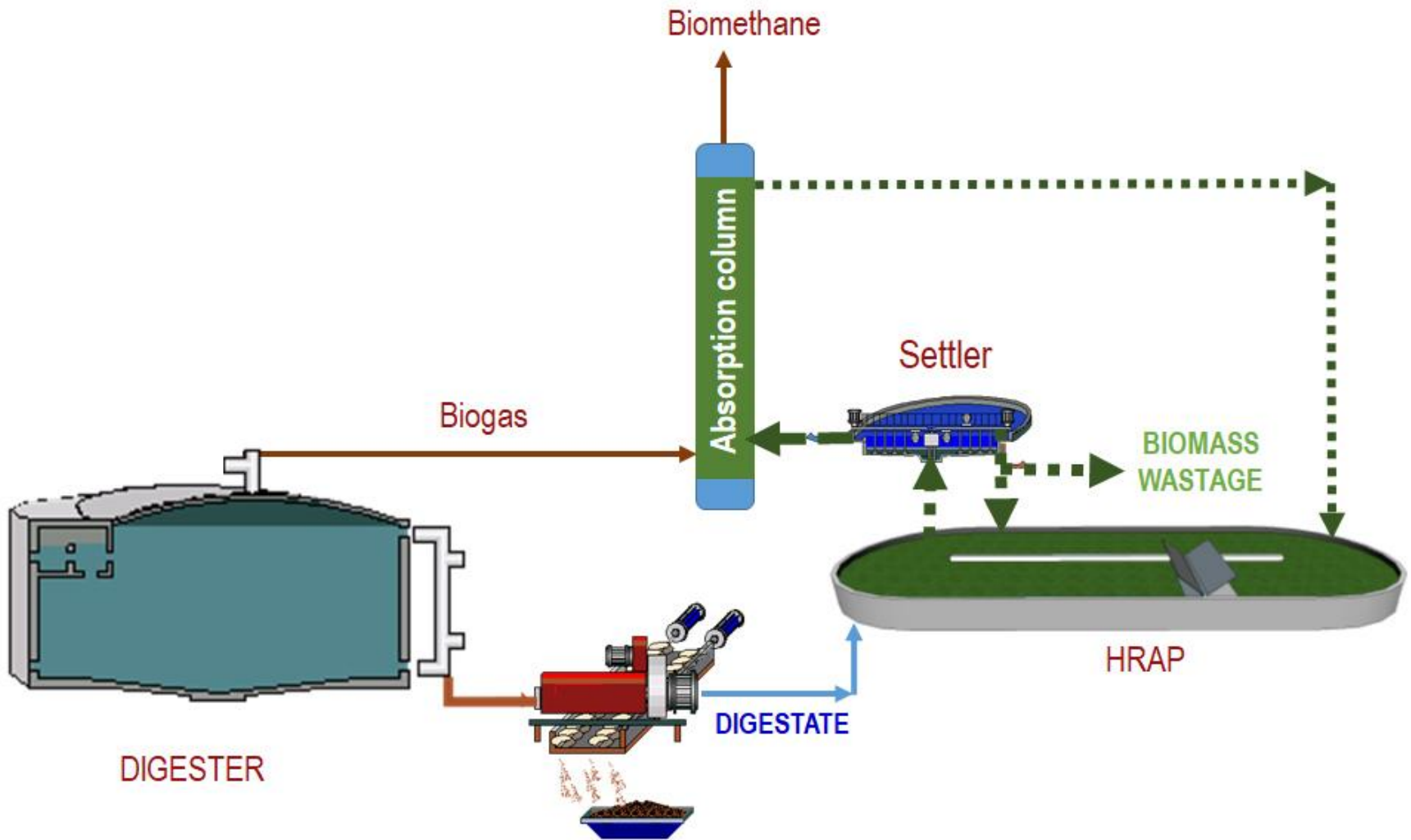
**Low Photosynthetic Efficiency** ↓ ↓

*Need to develop new operational strategies to operate biogas upgrading processes with digestates*





# Photosynthetic Biogas Upgrading & Nutrient Recovery



Contents lists available at ScienceDirect

**Algal Research**

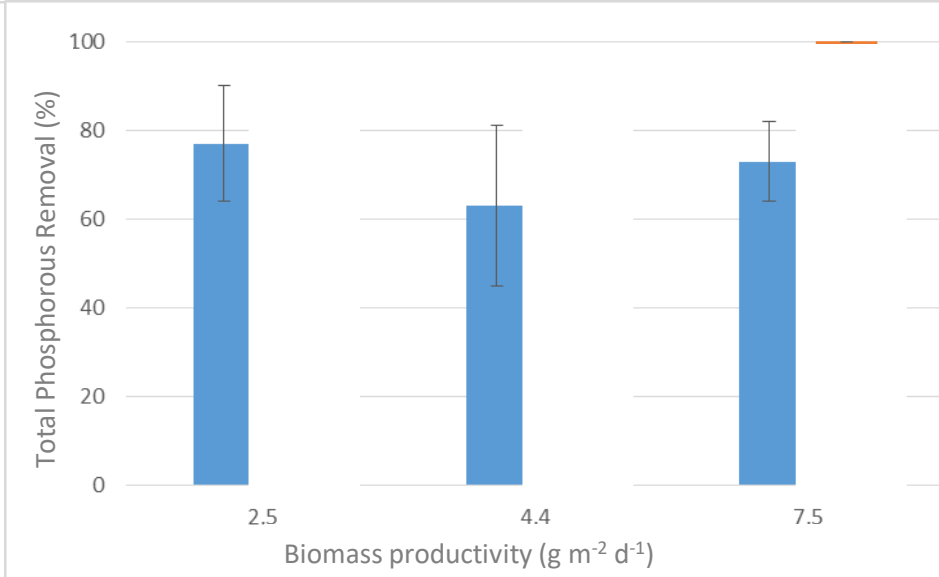
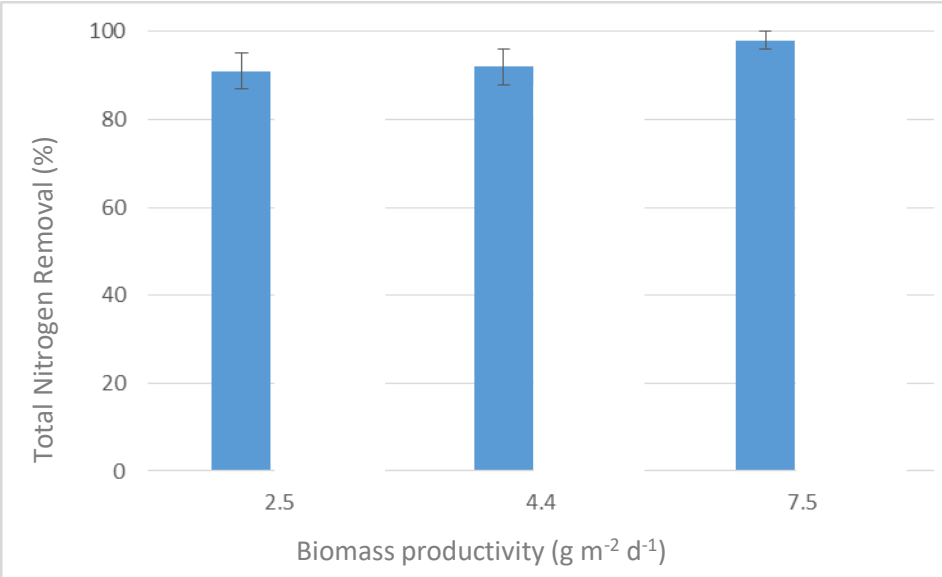
ELSEVIER journal homepage: [www.elsevier.com/locate/algal](http://www.elsevier.com/locate/algal)

algal

Photosynthetic biogas upgrading to bio-methane: Boosting nutrient recovery via biomass productivity control

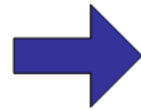
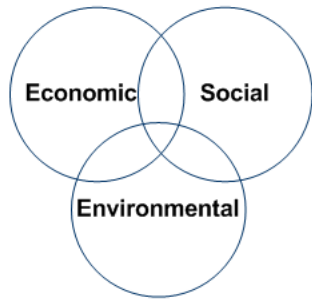
Alma Toledo-Cervantes<sup>a</sup>, Mayara L. Serejo<sup>b</sup>, Saúl Blanco<sup>c,1</sup>, Rebeca Pérez<sup>a</sup>, Raquel Lebrero<sup>a</sup>, Raúl Muñoz<sup>a,\*</sup>

CrossMark

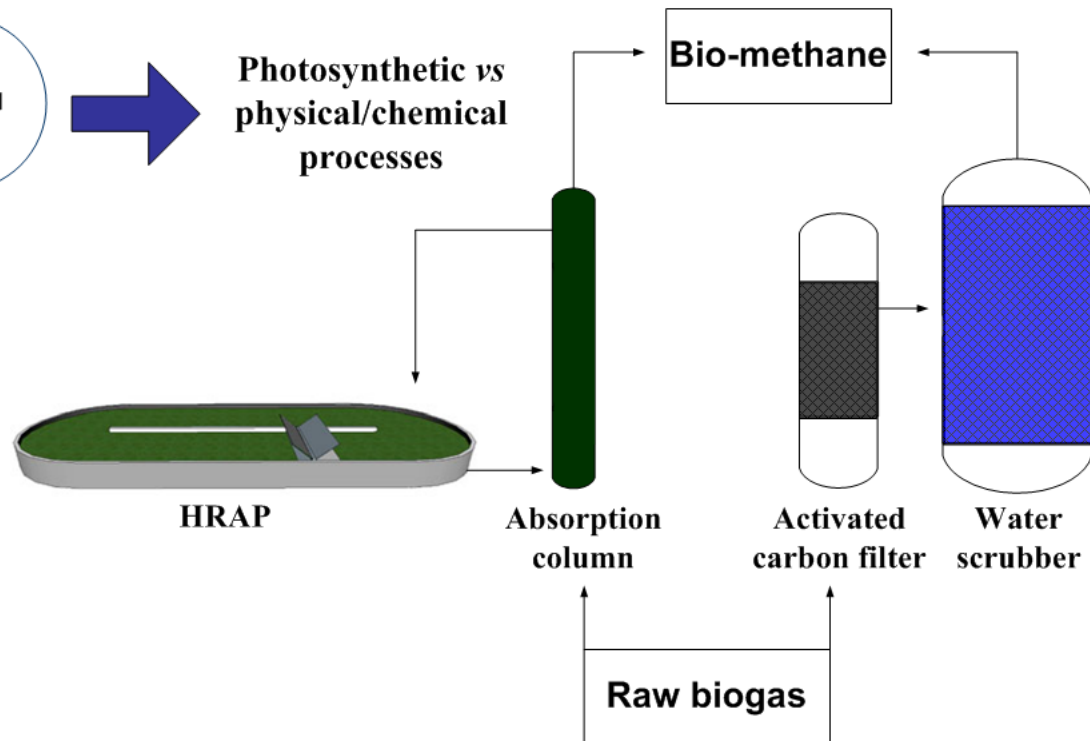


 Removal

## IChemE Sustainability Metrics



Photosynthetic vs  
physical/chemical  
processes

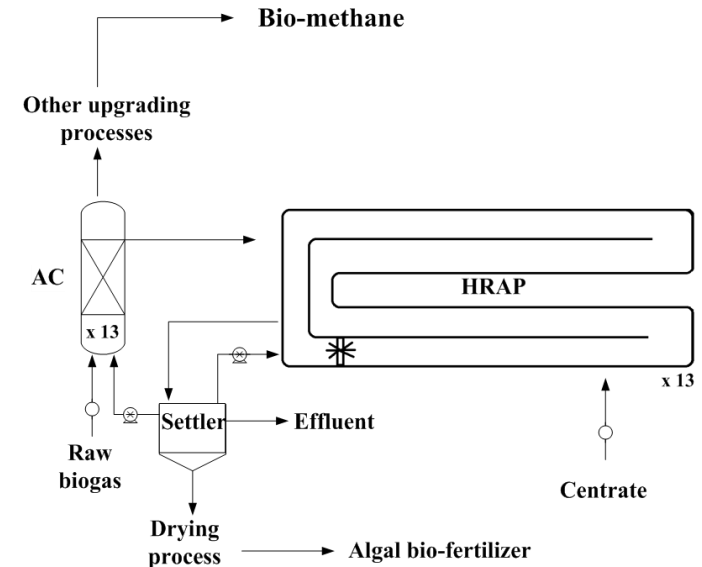
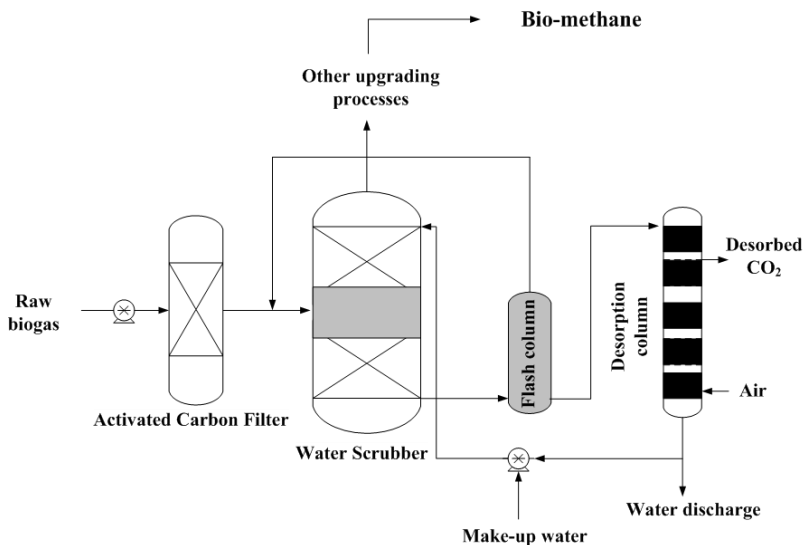


REFERENCE FLOW RATE: 300 Nm<sup>3</sup>/h

## Activated Carbon + Water Scrubber

Versus

## Photosynthetic Biogas Upgrading



**Table S1.** Investment costs of a ACF-WS for the upgrading of 300 Nm<sup>3</sup> h<sup>-1</sup> of biogas

	Cost	Units	Total cost (€)	References
<b>Land</b>	100	€ m <sup>-2</sup>	10 000	INE, 2015
<b>Activated carbon filter</b>	129	€ (Nm <sup>3</sup> /h) <sup>-1</sup> treated biogas	38 766	Xiao <i>et al.</i> (2008)
<b>Water scrubber</b>	3500	€ (Nm <sup>3</sup> /h) <sup>-1</sup> treated biogas	1 050 000	SGC Rapport 2013:270

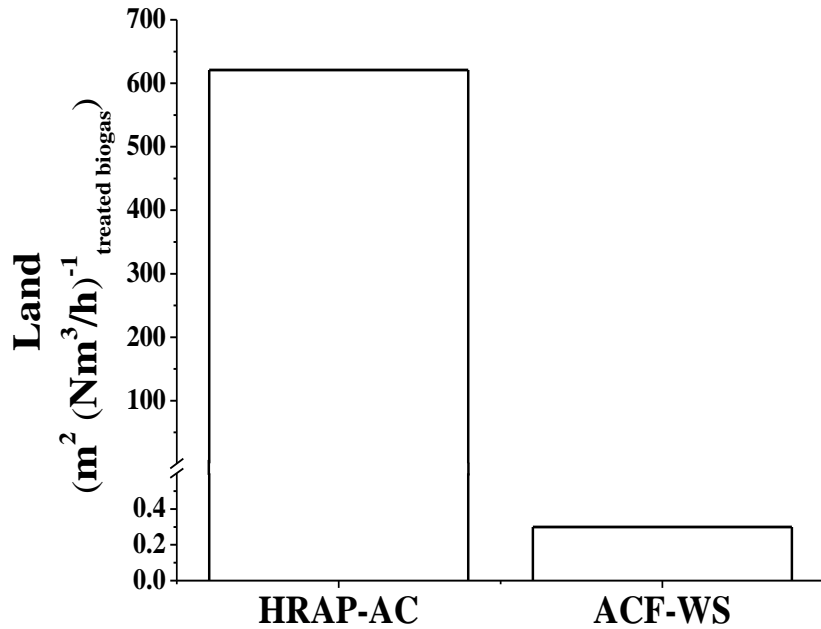
**Table S2.** Investment costs of the HRAP-AC for the upgrading of 300 Nm<sup>3</sup> h<sup>-1</sup> of biogas

	Cost	Units	Total costs (€)	References
<b>Land</b>	10 127	€ ha <sup>-1</sup>	188 712	MAGRAMA, 2014
<b>HRAP construction</b>	26 616	€ ha <sup>-1</sup>	356 382	Craggs <i>et al.</i> , 2012; Lundquist <i>et al.</i> , 2010
<b>Paddlewheel stations</b>	35 400	€ ha <sup>-1</sup>	474 006	Craggs <i>et al.</i> , 2012;
<b>Screw press</b>	86 000	€ unit <sup>-1</sup>	86 000	HUBER Technology, Germany
<b>Solar dryer</b>	325 000	€ unit <sup>-1</sup>	650 000	HUBER Technology, Germany
<b>AC</b>	3 980	€ unit <sup>-1</sup>	51 745	Delf Grupo España S.L.
<b>Gas diffusers</b>	250	€ (10 units) <sup>-1</sup>	3 250	Xylem Inc.



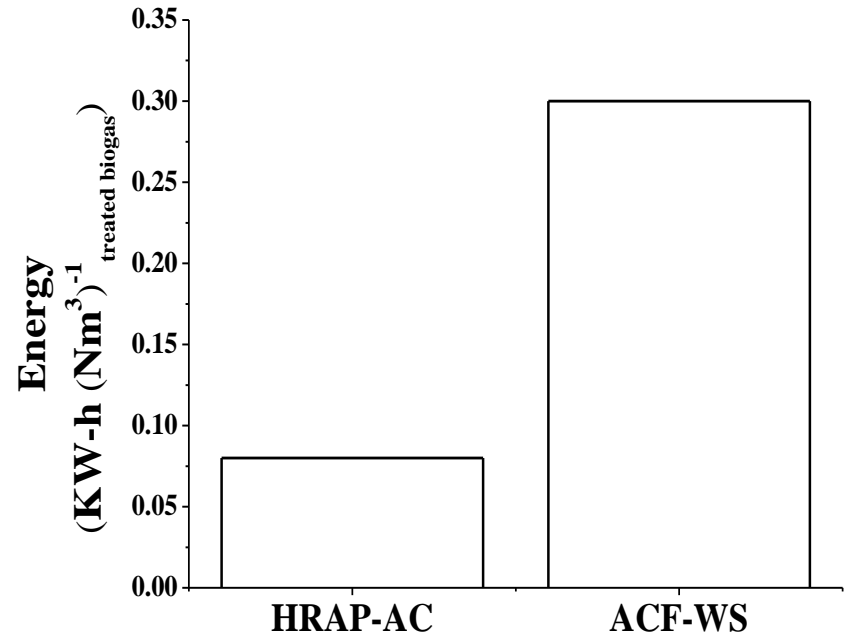
## Land Requirements

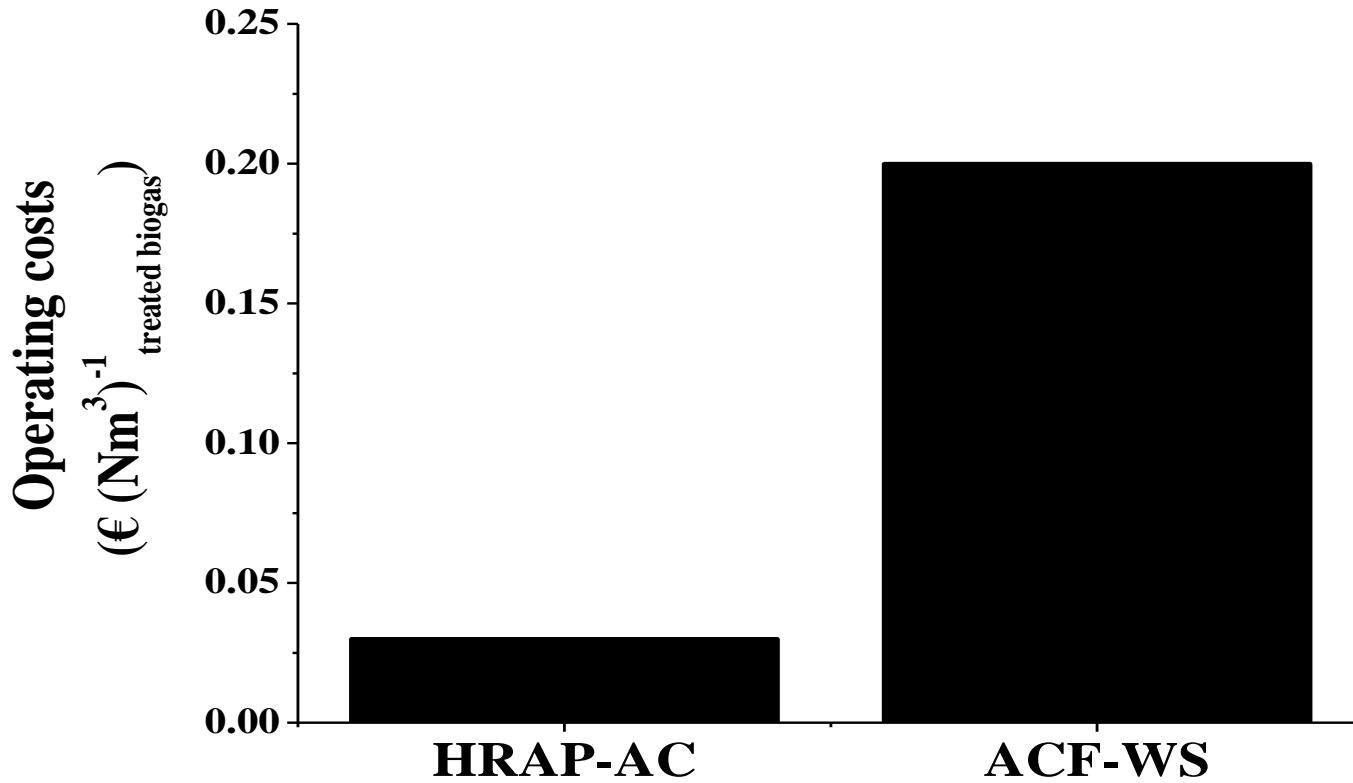
a)



## Energy Consumption

b)





### Biogas Upgrading market dominated by physical/chemical Technologies → High Operating Cost & Environmental Impact

✓ Algal-Bacterial Processes have shown a similar  $\text{CO}_2$  and  $\text{H}_2\text{S}$  removals & high robustness but with:

- Lower operating costs and **environmental impacts**
- No need for previous removal of particles/ $\text{H}_2\text{O}$ /siloxanes
- Tested at pilot scale
- Nutrient recovery from digestate

✓ Photosynthetic upgrading allows for simultaneous  $\text{H}_2\text{S}$  &  $\text{CO}_2$  removal

✓ Alkalinity, pH and L/G identified as key operational parameters

✓ Process control entails high process robustness

# Thank you for your Attention

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